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**Models for Calculating the Effects
of Isotopic Exchange, Radioactive Decay,
and of Recycle in Removing Iodine
from Gas and Liquid Streams**

Wallace Davis, Jr.

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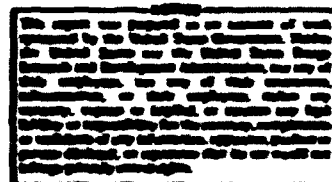
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**MODELS FOR CALCULATING THE EFFECTS OF ISOTOPIC EXCHANGE,
RADIOACTIVE DECAY, AND OF RECYCLE IN REMOVING IODINE
FROM GAS AND LIQUID STREAMS**

Wallace Davis, Jr.

SEPTEMBER 1975

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ABSTRACT

Different decontamination factors for ^{129}I and ^{131}I are frequently invoked in environmental impact reports concerned with nuclear fuel recycle. Selected differences, or ratios, have not been justified on the basis of mathematical models or experimental data. This report presents a description of the origins of these differences in terms of isotopic exchange and material balance equations for the short- and long-lived (or stable) isotopes. The ratios of decontamination factors can be calculated when there is complete attainment of isotopic exchange between gas- or liquid-phase iodine and iodine sorbed by a solid or liquid. If there is no exchange, decontamination factors are isotope-independent unless material recycle occurs within the system. Between these extremes, there can be decontamination factors whose explanation requires experimental determination of the extent of exchange. The model applies to other radioactive isotopes of iodine as well as to other elements with short- and long-lived (or stable) isotopes.

1. INTRODUCTION

The extents to which the iodine isotopes ^{129}I and ^{131}I are removed from gaseous or liquid streams by various treatment systems are frequently presumed to be different. For example, Yarbrow¹ presents retention factors of 20 and 40 for ^{129}I and ^{131}I , respectively, based² on the buildup and revaporization of iodine from solutions; such revaporization might reduce the ^{129}I retention relative to ^{131}I by a factor of 2 to 10. Staff members of Allied-General Nuclear Services³ have presented retention factors in the ratio 5/1 (favoring the retention of ^{131}I); two survey reports^{4,5} assign decontamination factors (DFs) of 3000 and 600 for ^{131}I and ^{129}I , respectively; and a more recent environmental impact analysis uses DFs of 750 and 75, respectively.⁶

These differences in retention of iodine isotopes are based on the recognition of radioactive decay of ^{131}I (half-life = 8.05 days) as an effective "decontamination" or "retention" factor which, however, does not apply to ^{129}I (half-life = 1.6×10^7 years); some of them are also based on the existence of pathways by which iodine can be recycled within fuel reprocessing plants, thereby effectively reducing decontamination factors. Although recycle and the qualitative difference between short- and long-lived isotopes have been used in analyzing the effectiveness of process equipment, such as silver zeolites, in retaining iodine, apparently no detailed description of the various factors has been given. The purpose of this report is to present such a description in terms of isotopic exchange, material balance equations, and material recycle, and to suggest methods for obtaining the few experimental data needed to ascertain the extent of exchange.

2. THE MODEL AND DEFINITIONS

While the model presented here applies to other elements and their isotopes, definitions are given in terms of a very small mass (a tracer quantity) of a short-lived isotope, ^{131}I , and a relatively very large quantity of nonradioactive isotopes of the same element. In this context, as well as for times less than 1000 years, ^{129}I is treated as "stable."

We consider iodine as one of the components of a gas stream entering a sorption system (see Fig. 1) that can chemically or physically trap a portion of the iodine. Silver zeolite beds and solutions of mercuric nitrate in nitric acid are examples of such systems. Iodine accumulates in the unit, which, eventually, must be regenerated or replaced when its sorption capacity starts to decrease or falls below some specified value. The following definitions apply:

- DF = equipment decontamination factor that applies to bulk iodine when the flow pattern is given by Fig. 1(a), Q_1/Q_2 ;
- DF^* = decontamination factor for ^{131}I , Q_1/Q_2 ;
- DF^S = decontamination factor for stable or long-lived isotope, Q_1/Q_2 [differs from DF when there is recycle, as in Fig. 1(b)];

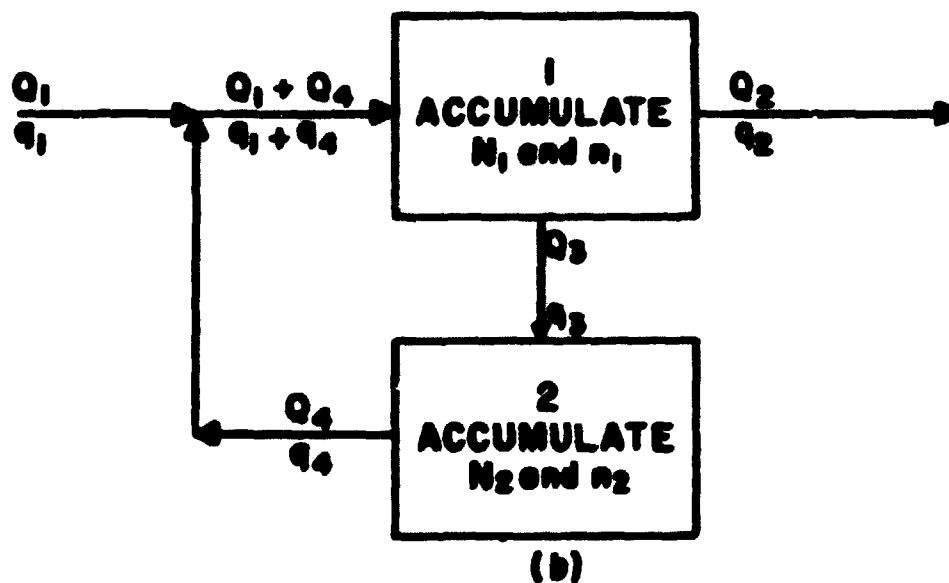
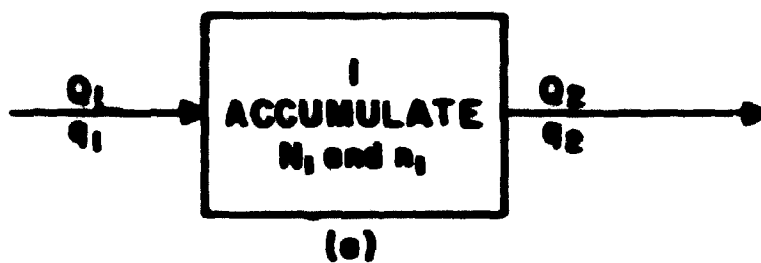


Fig. 1. Flow and accumulation diagrams for sorption units.
(a) Without recycle; (b) With one form of recycle.

- ⁰ = superscript to refer to a value at the zero reference time;
- f = fractional attainment of equilibrium isotopic exchange between the gas-phase atoms of iodine in the sorber and those "fixed" on the sorbent before some of the atoms leave the sorber ($0 \leq f \leq 1$);
- $k = q_1 [1 - (1 - f)Q_2/Q_1]$, a combined rate, constant or time-dependent, applicable to Fig. 1(a), day^{-1} ;
- n_1 = number of atoms, or gram-atoms, of ^{131}I "fixed" more or less tightly in the sorbent;
- N_1 = number of all atoms, or gram-atoms, of iodine that are "fixed" more or less tightly in the sorbent;
- q_1 = the rate, constant or time-dependent, at which ^{131}I enters the sorber, atoms/day or gram-atoms/day (or other time unit);
- Q_1 = the rate, considered to be essentially constant (the bulk of the iodine is stable or long-lived ^{127}I), at which all iodine enters the sorber, atoms/day or gram-atoms/day;
- q_2 = the rate at which ^{131}I leaves the sorber, atoms/day or gram-atoms/day;
- Q_2 = the rate at which all iodine leaves the sorber, atoms/day or gram-atoms/day;
- q_3 = the rate at which ^{131}I leaves the sorption unit [Fig. 1(b)] to report to a holdup tank, atoms/day or gram-atoms/day;
- Q_3 = the rate, constant or time-dependent, at which iodine leaves the sorption unit 1 [Fig. 1(b)] to report to a holdup tank, atoms/day or gram-atoms/day;
- q_4 = the rate at which ^{131}I is recycled to the sorption unit, atoms/day or gram-atoms/day;
- Q_4 = the rate at which iodine is recycled to the sorption unit, atoms/day or gram-atoms/day;
- t = time, days or any other appropriate unit;
- λ = the decay constant of the short-lived species, day^{-1} (or reciprocal of time if another time unit is used) = 0.0861 day^{-1} for ^{131}I ;
- $t_{1/2}$ = half-life of short-lived isotopes, 8.05 days in the case of ^{131}I .

3. NUCLEAR FUEL REPROCESSING

Calculations presented in this report are based on material balance equations and isotopic exchange (which may vary from 0 to 100% in degree of completeness). The material balance equations can be quite numerous, depending on the complexity of the sorption and recycle systems used in a nuclear fuel reprocessing plant to reduce the quantities of iodine, or other element with radioactive isotopes, discharged to the environment. Only two types of sorption systems are analyzed in this report. The first, Fig. 1(a), is a no-recycle system; the second involves recycle in the system shown in Fig. 1(b).

3.1 Sorption Without Recycle

In this case, the material-balance equations for ^{131}I and total iodine entering and leaving a sorbent bed may be written as:

$$dn_1/dt = Q_1 - Q_2 - \lambda n_1, \quad (1)$$

and

$$dN_1/dt = Q_1 - Q_2 - \lambda n_1. \quad (2)$$

The term λn_1 in these equations accounts for the loss, by decay, of ^{131}I .

Before extending the mathematical analysis of Eqs. (1) and (2), it is worth noting the magnitudes of the several flow rates. As summarized in Table 1, typical values of the average rates, Q_1 , at which all iodine species will report to the primary iodine-removal units in plants reprocessing light-water reactor (LWR) fuels, high-temperature gas-cooled reactor (HTGR) fuels, and liquid-metal-cooled fast breeder reactor (LMFBR) fuels will be about 10 g-atoms/day. The stable isotope ^{127}I and the long-lived ^{129}I (half-life = 1.6×10^7 years) contribute nearly all the mass of Q_1 . Similarly, the flow of ^{131}I , Q_2 , into the primary iodine removal units is in the order of 10^{-7} g-atom/day into LWR and HTGR fuel reprocessing plants, at reprocessing time, and 10^{-6} g-atom/day into the primary sorber of the LMFBR fuel reprocessing plant. If decontamination factors (DFs) for these units are in the order of 10 to 100, the flow,

Table 1. Expected rates of flow of iodine isotopes in LWR, HTGR, and LMFBF fuel reprocessing plants

Flow rate	Type of reactor fuel processed		
	LWR ^a	HTGR ^b	LMFBR ^c
¹³¹ I, Ci/day	4.6	2.5	4.0×10^3
Q_1 , g-atoms/day	2.8×10^{-7}	1.5×10^{-7}	1.9×10^{-4}
¹²⁹ I, g-atoms/day	8.9	8.8	10.2
Total I, Q_1 , g-atoms/day	10.5	11.0	12.5

^aBased on averages from Tables 4.2 and 4.5 of ref. 7 for fuel 160 days after discharge from the reactor. Original output from the ORIGEN code⁸ was used as the source of gram-atoms per metric ton of heavy metal (MTHM). The capacity of the LWR fuel reprocessing plant is assumed to be 1500 MTHM/year.

^bBased on Table 4.8 of ref. 7 for fuel 160 days after discharge from the reactor. Original output from the ORIGEN code⁸ was used as the source of gram-atoms/MTHM. The capacity of the HTGR fuel reprocessing plant is assumed to be 450 MTHM/year.

^cBased on Table 4.14 of ref. 7 for fuel 90 days after discharge from the reactor. Original output from the ORIGEN code⁸ was used as the source of gram-atoms/MTHM. The capacity of the LMFBF fuel reprocessing plant is assumed to be 1500 MTHM/year.

Q_2 , of total iodine out of the primary sorber would be in the range 0.1 to 1 g-atom/day for all of the fuel reprocessing plants; the flows, Q_3 , of ¹³¹I out of the primary sorbers would be in the range 10^{-9} to 10^{-8} g-atom/day in LWR and HTGR fuel reprocessing plants and 10^{-6} to 10^{-5} g-atom/day in the LMFBF fuel reprocessing plant.

The amount, n_1 , of ¹³¹I retained within a sorbent will be calculated below; however, it is easy to demonstrate that, because of decay, the inventory of this nuclide will not exceed that which flows into the sorbent over a period $t_{1/2} / \ln 2$ (about 11.6 times the daily input rate in the case of ¹³¹I). Therefore, n_1 will be less than 3.3×10^{-6} , 1.7×10^{-6} , and 2.2×10^{-3} for LWR, HTGR, and LMFBF fuel reprocessing plants, respectively; the product λn_1 is less than the rate at which ¹³¹I enters the plant (Table 1). It is apparent, therefore, that λn_1 will be much smaller than

Q_1 or Q_2 for the primary iodine-removal unit of fuel reprocessing plants. [Exceptions to this occur if DF is $\geq 10^5$ for the LMFR fuel reprocessing plant or $\geq 10^7$ for LWR or HTR fuel reprocessing plants; in such instances, $\lambda n_1(\max)$ and Q_2 could be nearly equal.] In this case, the term λn_1 could be deleted from Eq. (2) without introducing significant errors, to give:

$$dn_1/dt = Q_1 - Q_2. \quad (3)$$

Integration of Eq. (3) leads to the very good approximation

$$n_1 = n_1^0 + (Q_1 - Q_2)t. \quad (4)$$

If no exchange occurred between fresh atoms entering the sorber and those already "fixed," the DFs for both ^{131}I and stable isotopes would be equal, and equal to the equipment DF, namely

$$DF^S = DF^* = DF = Q_1/Q_2 = Q_1/Q_2; \quad (5)$$

and

$$Q_2 = (Q_1/Q_2)Q_2. \quad (6)$$

If there is complete exchange between atoms in the gas phase and condensed phase in the sorber,

$$Q_2 = (n_1/N_1)Q_2. \quad (7)$$

More generally, for a fractional exchange, f ,

$$Q_2 = [(1-f)(Q_1/Q_2) + f(n_1/N_1)]Q_2. \quad (8)$$

On substituting Eq. (8) into Eq. (1), we obtain:

$$dn_1/dt = Q_1 - [(1-f)(Q_1/Q_2) + f(n_1/N_1)]Q_2 - \lambda n_1. \quad (9)$$

Rearrangement of Eq. (9) yields:

$$dn_1/dt + (\lambda + fQ_2/N_1)n_1 = Q_1[1 - (1-f)Q_2/Q_1]. \quad (10)$$

In general, a simple, closed-form solution of Eq. (10) does not exist; however, in several important cases, n_1 may be approximated adequately by a closed-form solution to a simplified form of Eq. (10).

In these cases, a desk calculator can be used to calculate DF^* , the decontamination factor for ^{131}I with a short half-life, as contrasted to values of DF^S , the decontamination factors for stable isotopes (^{127}I) or those with long half-lives (e.g., ^{129}I), which will equal DF .

After an initial shakedown, or startup, period, nuclear fuel reprocessing plants are expected to approach a type of steady state in operations wherein the activity of each radioactive nuclide in spent fuel reporting to head-end operations becomes more or less constant. This condition corresponds to both

$$Q_1 = \text{constant} \quad (11a)$$

and

$$Q_2 = \text{constant} . \quad (11b)$$

Typical values of Q_1 for ^{131}I and of Q_2 for ^{129}I and the stable ^{127}I for expected operations in LWR, HTGR, and LMFR fuel reprocessing plants are listed in Table 1.

The system of differential equations described in Eqs. (1) and (2) was integrated numerically using the classical fourth-order Runge-Kutta procedure. Appendix A contains a listing of the FORTRAN-IV program except for the Runge-Kutta subroutine, RK4DEQ, of Nestor.⁹ Results of calculations in which only DF was varied and the other parameters were held constant are summarized in Fig. 2. It is apparent that, for any particular DF^S ($= DF$) for bulk iodine (^{129}I or ^{127}I), the value DF^* for ^{131}I will continue to increase with time as long as complete isotopic exchange occurs; alternatively, if the measured DF^* for ^{131}I is constant, the DF^S for ^{129}I or ^{127}I must be decreasing as long as any isotopic exchange occurs.

The extent of exchange is an important parameter, as shown in Figs. 3 and 4; however, there do not appear to be any data which can be used to test the model of this report and to yield a value for this parameter. The data of Ackley and Davis,¹⁰ discussed below, imply that nearly complete isotopic exchange was achieved in their experiments on trapping of iodine on silver zeolite. "Nearly complete" might mean a value of f as low as 0.8 (perhaps lower) or as large as 1 because of the uncertainties in the experimental values of DF^* .

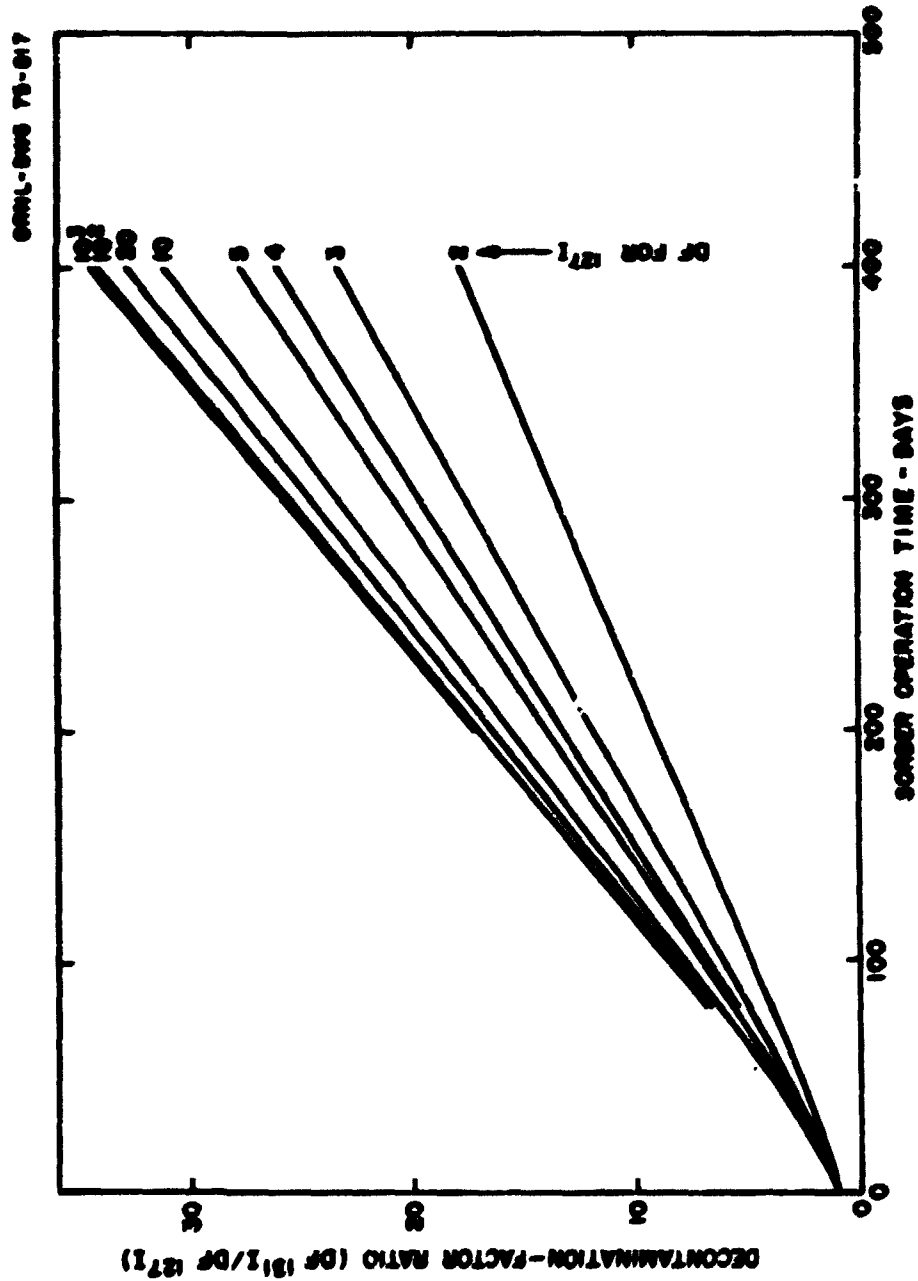


Fig. 2. Effects of time and equipment DF on the ratio $\text{DF } ^{131}\text{I}/\text{DF } ^{127}\text{I}$. Flow pattern is given in Fig. 1(a); $f = 1$.

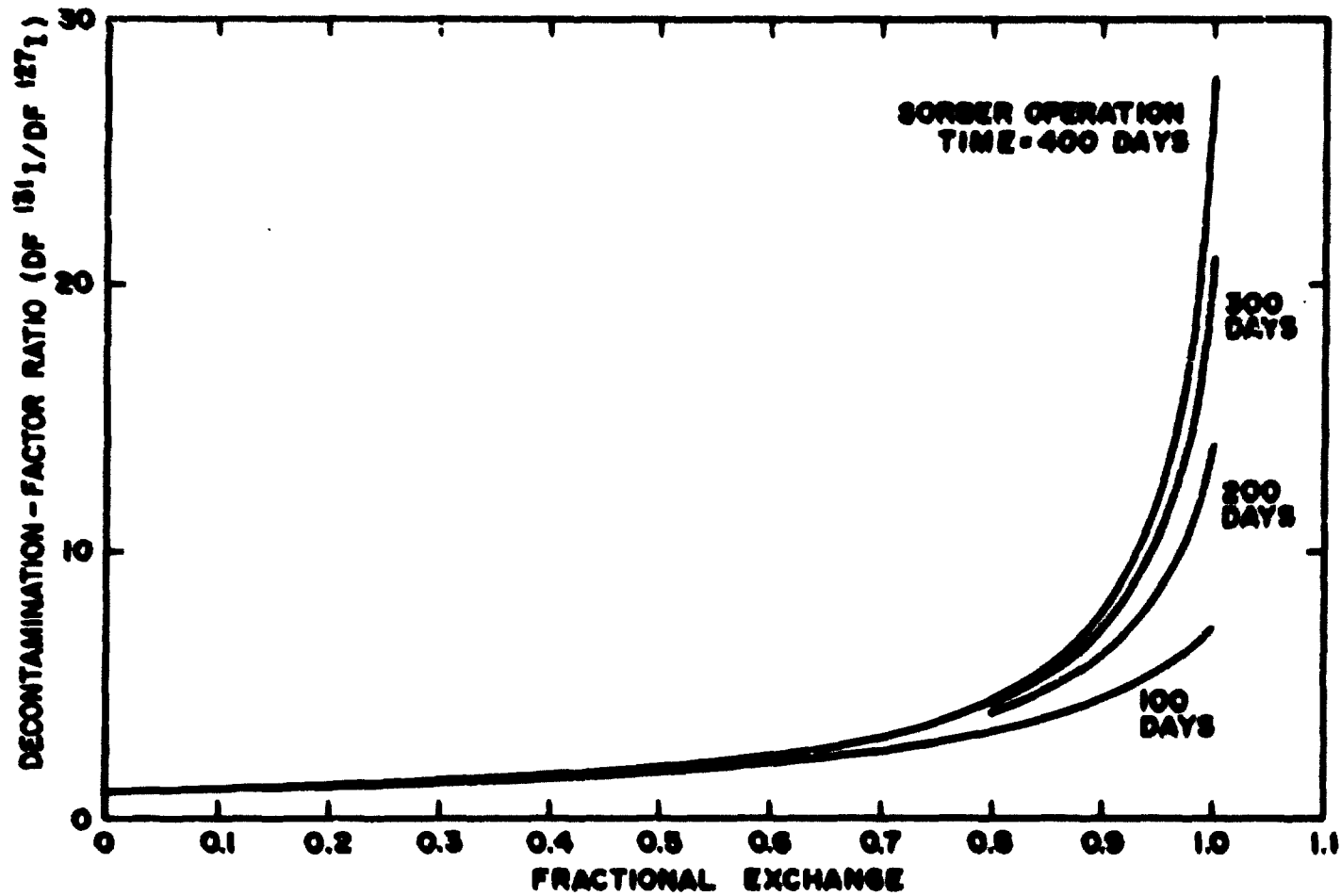


Fig. 3. Effects of fractional exchange and time on the ratio $\text{DF } ^{131}\text{I}/\text{DF } ^{127}\text{I}$. Flow pattern is given in Fig. 1(a); $\text{DF (equipment)} = 5$.

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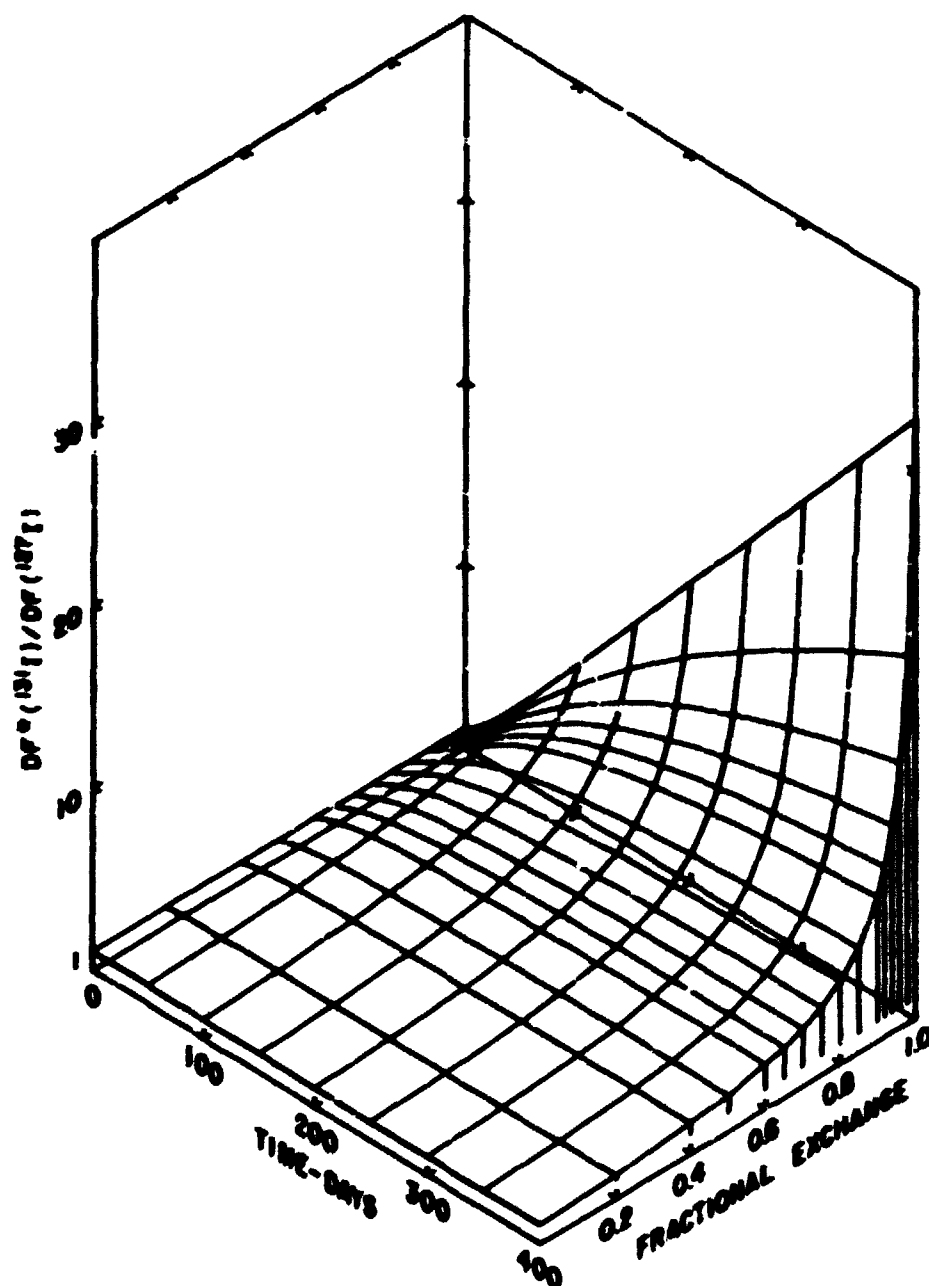


Fig. 4. Effects of time and fractional exchange on the ratio $DF^{131}I / DF^{127}I$. Flow pattern is given in Fig. 1(a).

As mentioned above, Eq. (10) has solutions that may be expressed in closed form for certain boundary conditions. One such situation occurs when $fQ_0/M_1 \ll \lambda$. For ^{131}I , $\lambda = 8.61 \times 10^{-2} \text{ day}^{-1}$. Thus, we refer to problems for which $fQ_0/M_1 = fQ_0/[M_1^0 + (Q_0 - Q_0)t] \ll 8.6 \times 10^{-2} \text{ day}^{-1}$. When $n_1^0 = 0$ and $M_1^0 = 0$, this requires that $(DF - 1)\lambda t \gg f$.

Such a condition is satisfied, for example, if DF^S (stable ^{127}I) exceeds 5 when $f = 1$ and the sorbent has been in use for 25 days or more; it is also satisfied even for a DF^S value as low as 2 after the bed has been in use for 100 days or more and f is as low as 0.5. For such conditions, Eq. (10) may be replaced with the simpler form

$$dq_1/dt + \lambda q_1 = k \quad (12)$$

The solution to this equation is:

$$q_1 = \frac{k}{\lambda} (1 - e^{-\lambda t}) \quad (13)$$

By substituting Eqs. (4) and (13) into Eq. (8), the quantity, q_2 , of ^{131}I leaving the sorbent is found to be:

$$q_2 = \left[(1 - f)(q_1/Q_0) + \frac{fQ_0[1 - (1 - f)Q_0/Q_0](1 - e^{-\lambda t})/\lambda}{(Q_0 - Q_0)t} \right] Q_0 \quad (14)$$

By using Eq. (5) to define the DF for bulk iodine and using

$$DF^* = q_2/q_1 \quad (15)$$

we obtain

$$DF^* = \frac{1}{\frac{(1 - f)}{DF} + \frac{f[1 - (1 - f)/DF](1 - e^{-\lambda t})}{(DF - 1)\lambda t}} \quad (16)$$

Equation (16) summarizes the model of isotopic exchange when $n_1^0 = 0$, $M_1^0 = 0$, and $fQ_0/M_1 \ll \lambda$. Two examples of its use are presented in the subsections that follow.

3.1.1 Values of DF^* for the case of no exchange

In this case, $f = 0$ and $DF^* = DF$ at all times.

3.1.2 Values of DF^* for the case of complete exchange

In this case, $f = 1$ and $DF^* = (DF - 1)\lambda t / (1 - e^{-\lambda t})$. Since $(DF - 1)\lambda t \gg 1$ in this example, we find that

$$DF^*/DF \approx 1/DF + (1 - 1/DF)\lambda t. \quad (17)$$

It may be seen from Fig. 2 that the ratio increases as the DF value or time increases; further, the intercepts are nearly $1/DF$ and the slopes of the linear portions of the curves ($t > 100$ days) are nearly $(1 - 1/DF)\lambda$, as required by Eq. (17). The ratio DF^*/DF is nearly independent of DF when $DF \geq 100$.

The ratios shown in Fig. 2 for $f = 1$ increase to about 10 for times in the order of 4 months. Both this factor of 10 and the time period are pertinent in analyzing the performance of process equipment. Expectations or observations of DF^*/DF in the order of 10 imply considerable exchange (80% or more) of ^{131}I with the massive quantities of ^{127}I and ^{129}I collected in sorbents; Fig. 2 shows that the factor should increase to approximately 30 after the equipment has performed at design values for a year or more. However, the absence of significantly better performance of a sorbent bed for ^{131}I than for ^{127}I almost certainly corresponds to a small degree (50% or less) of isotopic exchange.

3.2 Sorption With Recycle

The mass-balance equations used in Sect. 3.1 pertain to a specific sorption system [Fig. 1(a)] whose design does not include provisions for recycle of the element of interest, such as iodine. Hence they are not applicable to the many cases of importance in nuclear fuel reprocessing where recycle is an integral step; each of these cases requires individual analysis. Besides the once-through sorption unit of Fig. 1(a), only one other type of sorption system is considered in this report, namely the recycle system of Fig. 1(b). In this system, iodine is sorbed up to

some maximum value, $M(\max)$; concurrently, part of the input iodine reports to a reservoir, 2(a waste tank), which may either be the final storage tank or a tank from which iodine can be sparged back to the sorption system. Differential equations needed to describe the system of Fig. 1(b) are more numerous and complicated than those needed to describe the system of Fig. 1(a); however, the calculations can easily be performed when a computer is available.

Using the definitions of Sect. 2, the equations to describe the system of Fig. 1(b) are as follows:

$$dM_1/dt = Q_1 - Q_2 - Q_3 + Q_4 - \lambda M_1, \quad (18)$$

$$dM_2/dt = Q_2 - Q_3 - \lambda M_2, \quad (19)$$

$$dM_3/dt = Q_3 - Q_4 - Q_5 + Q_6 - \lambda M_3, \quad (20)$$

$$dM_4/dt = Q_5 - Q_6 - \lambda M_4. \quad (21)$$

It is apparent that Eqs. (18) and (20) reduce to Eqs. (2) and (1), respectively, when $Q_2 = Q_3 = 0$.

Equations (18)-(21) can be analyzed only after some boundary conditions have been specified. These conditions may be represented in various ways, such as the flow rates shown for two concepts in Fig. 5. This figure is based on the use of a maximum capacity of the sorbent to trap iodine and on the continuous discharge (as from a mercuric nitrate scrubber discharging to a waste tank) of part of the trapped iodine. The particular example analyzed in this report is based on two assumptions:

- (1) The iodine leaves trap 1 and reports to storage tank 2 at a rate given by

$$Q_2 = M_1 U, \quad (22)$$

where the rate constant U is defined as

$$U = \ln 2/T_{1/2} \quad (23)$$

and $T_{1/2}$ is the time required for half the capacity of the sorbent 1 to be expended, perhaps 60 days.

- (2) The amount of iodine recycled from unit 2 to the main stream is proportional to the amount of iodine contained in unit 2. In this case,

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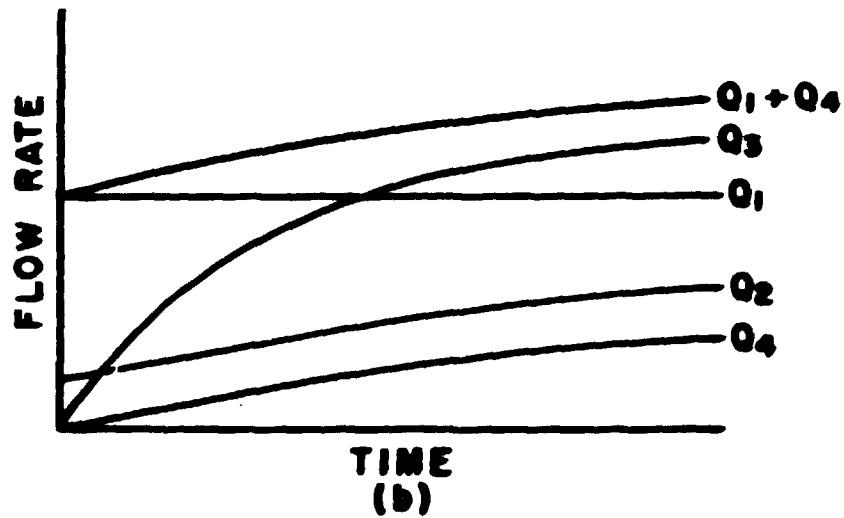
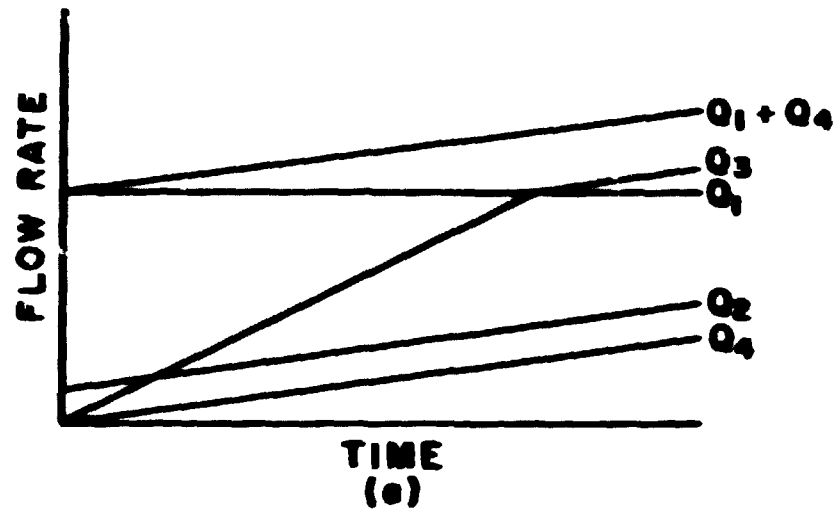


Fig. 5. Two types of flow patterns for the recycle system shown in Fig. 1(b).

$$Q_2 = RN_2 \quad (24)$$

Since trap 1 is assumed to have a maximum capacity, $N(\max)$, the maximum flow of iodine to tank 2 is

$$Q_2(\max) = N_1(\max) U \quad (25)$$

This occurs when trap 1 is saturated with iodine,

$$dN_1/dt = 0 \quad , \quad (26)$$

in which case

$$Q_2 = Q_2(\max) = Q_1 - Q_3 + Q_4 - \lambda n_1 \quad (27)$$

and

$$Q_2(\max) = (Q_1 + Q_3)(1 - 1/DF) - \lambda n_1 \quad (28)$$

Using Eqs. (22) and (25),

$$Q_2/Q_2(\max) = N_1 U / [N_1(\max) U] \quad (29)$$

Thus

$$Q_2 = [N_1/N_1(\max)] [(Q_1 + Q_3)(1 - 1/DF) - \lambda n_1] \quad (30)$$

In this same example, we use

$$Q_3 = (n_2/N_2) Q_2 \quad (31)$$

$$Q_4 = (n_3/N_3) Q_2 = RN_3 \quad (32)$$

and

$$Q_2 = [(1 - f)(Q_1 + Q_3)/(Q_1 + Q_3) + f(n_2/N_2)] Q_2 \quad (33)$$

Equations (18)-(33) form the basis of the computer program listed in Appendix A; this program produced the results shown in Figs. 2-4 for a system in which there is no recycle of iodine; it produced the results shown in Fig. 6(a) and 6(b) for a system with recycle.

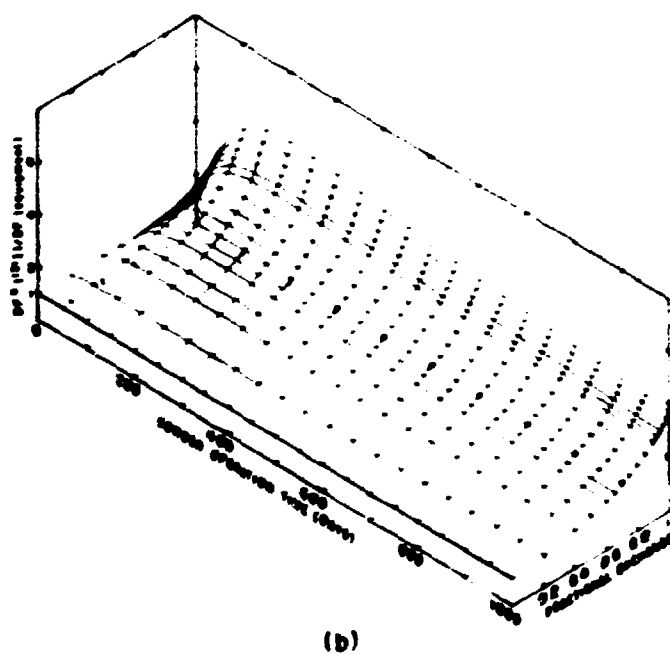
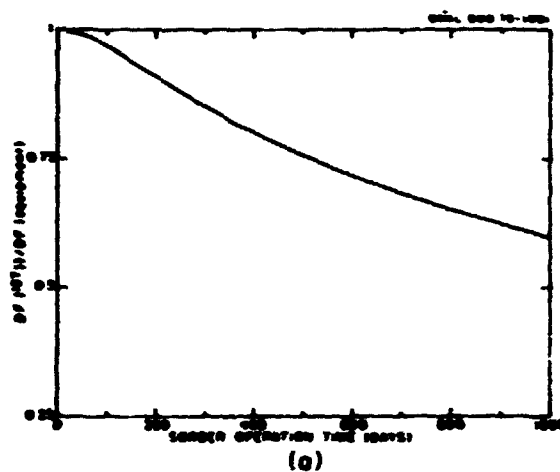


Fig. 6. Effects of time, recycle, and fractional exchange on relative decontamination factors. (a) For ^{127}I ; (b) for ^{121}I . In both cases, $DF(\text{equipment}) = 20$, $T_{N(\text{max})} = 60$ days, $R = 1 \times 10^{-3}$.

4. LABORATORY EXPERIMENTS

Many laboratory studies, such as those of Ackley and Davis,¹⁰ lend themselves to testing the model proposed in this report. In such studies, a quantity of stable iodine is spiked with tracer iodine, such as ^{128}I , ^{130}I , or ^{131}I , which is passed through a sorbent bed until its level of radioactivity becomes too low for accurate counting. In contrast to the situation in Sect. 3, the quantity q_1 in these experiments is, therefore, time-dependent according to the relation

$$q_1 = q_1^0 e^{-\lambda t} ; \quad (34)$$

and Eq. (10) becomes

$$dn_1/dt + (\lambda + fQ_0/M_1)n_1 = k^0 e^{-\lambda t} , \quad (35)$$

where

$$k^0 = q_1^0 [1 - (1 - f)Q_0/q_1] . \quad (36)$$

Equation (36) can be integrated analytically to yield

$$n_1 = \left\{ \left(n_1^0 - \frac{q_1^0 M_1^0}{Q_0} \right) \left[\frac{M_1^0}{M_1} \right]^{\frac{fQ_0}{(Q_1 - Q_0)}} + \frac{q_1^0 M_1}{Q_0} \right\} e^{-\lambda t} . \quad (37)$$

Finally, the quantity DF^* is calculated as

$$DF^* = \frac{q_1}{Q_0} = \frac{q_1^0 e^{-\lambda t}}{Q_0} = \frac{DF}{1 + \frac{f}{M_1} \left[\frac{M_1^0 Q_0}{q_1^0} - M_1^0 \right] \left[\frac{M_1^0}{M_1} \right]^{\frac{f}{(DF-1)}}} . \quad (38)$$

As examples of the application of the model presented here, either by use of Eqs. (1) and (2), Eq. (10), or Eq. (37), we reanalyze data from Tables 1 and 2 of ref. 10 pertaining to the sorption of iodine by a 26% (Ag^+ for Na^+ exchanged) silver zeolite. The following data are derived from these tables, in the nomenclature of this report. An air stream containing I_2 with tracer ^{128}I ($t_{1/2} = 60$ days) was passed into each of ten test beds for 196 days. At the end of this period, each bed loading was 4.02 mg/ml. The radioactivity level of the tracer was then increased about 500 times and the experiment continued. Samples were taken 90

and 154 days after the ^{128}I activity had been increased, that is, at total elapsed times of 286 and 350 days. Loadings at these times were 7.01 and 9.19 mg/ml, respectively. The flow of I_2 was stopped occasionally during the first 286 days of these experiments, and CH_3I with ^{130}I tracer ($t_{1/2} = 12.4$ hr) was injected instead. By this method, sorption of both I_2 and CH_3I on the same bed was measured.

In applying Eqs. (37) and (38) to the first 196 days of I_2 sorption, we use the condition that the bed initially contained no iodine. This is equivalent to:

$$n_1^0 = n_2^0 = 0 \quad (39)$$

This condition allows Eq. (37) to be simplified to:

$$n_1 = q_1^0 (1 - 1/DF) e^{-\lambda t} \quad (40)$$

and the rate at which ^{128}I was discharged from the bed is given, by use of Eqs. (8), (18), and (40), as

$$q_2 = q_1^0 e^{-\lambda t} / DF \quad (41)$$

The expected result is obtained when $q_1 (= q_1^0 e^{-\lambda t})$ is divided by q_2 ; that is,

$$DF^* = DF$$

for all values of f . Thus, the model does satisfy one expected condition, namely, the decontamination factor obtained for the tracer is the same as that for the bulk iodine, regardless of how complete the exchange might be, as long as a single batch of traced iodine is being used.

When a new batch of traced iodine is used in a system previously exposed to this element, but at a different specific radioactivity of tracer, the decontamination factor for the tracer generally no longer equals the DF for bulk iodine. Instead, $DF^* > DF$ if the specific radioactivity of the new batch is higher than that of the previous one, and $DF^* < DF$ if it is less. The reason for these inequalities may be seen by examining the term $(n_1^0 q_2 / q_1^0 - n_2^0)$ of Eq. (38). Tracer and bulk

iodine inventories of the sorbent at the end of the usage of one batch of sorbate are n_1^0 and M_1^0 , respectively. If the bulk iodine flow rate, Q_1 , is held constant, an increase in the tracer activity corresponds to an increase in q_1^0 , to a decrease in $(n_1^0 Q_1 / q_1^0 - M_1^0)$ and, therefore, to an increase in DF^* according to Eq. (38). On the other hand, changing to a sorbate with lower activity corresponds to a decrease in q_1^0 , to an increase in $(n_1^0 Q_1 / q_1^0 - M_1^0)$ and, hence, to a decrease in DF^* .

Experiments are performed with tracers to utilize particle or photon counting techniques, which are usually much more accurate than normal chemical techniques, especially for obtaining the rate at which a trapped species leaves a highly efficient sorbent bed. Equation (38) cannot be rearranged to solve directly for the bulk-iodine DF for the measured tracer DF^* ; instead, it is necessary to solve for DF by iterative methods. This can be done with a desk calculator or with the short computer program presented in Appendix B.

Using Eq. (38), a reanalysis of the data of Ackley and Davis¹⁰ pertaining to sorption of iodine by the 26% (Ag^+ for Ka^+ exchanged) silver zeolite after the first 196 days of exposure, that is, after changing to iodine with a higher ^{128}I specific activity, shows that DF^* increased for constant DF . Some of the calculated values derived from Eq. (38) are listed in Table 2. The DF^*/DF ratio, which is in excess of 2.3 after 286 days of exposure and nearly 1.8 at 350 days, is of particular interest. By contrast, Ackley and Davis estimated this ratio to be in the order of 4. Specific activities of sorbed inlet and exit gas-phase iodine, in millicuries per gram of iodine, are also listed in Table 2. Since 100% exchange was assumed, the sorbed-phase specific activity and exit gas-phase activity are equal.

Many of the data in ref. 10 show DF^* s for tracer iodine that were too high to measure with the particular specific activity in use. In the example reanalyzed here, the DF^* s with the original traced iodine were 1×10^6 and 5×10^3 at 35 and 77 days, respectively; at 140 and 196 days, the DF^* s were too large to determine with the low specific activity of ^{128}I in stable iodine. These tracer DF^* s are equal to the bulk DF s, as explained above. Data obtained with the higher-activity iodine, introduced

Table 2. Calculations of DF^3 for stable ^{127}I from DF^* values for ^{128}I of Ackley and Davis¹⁰

Exposure History Through 196 Days			
n_1 , inventory of ^{128}I , g-atoms	1.04E-13		
N_1 , inventory of $^{128}\text{I} + ^{127}\text{I}$, g-atoms	9.01E-04		
n_1/N_1 , inventory ratio	1.16E-10		
Specific activity, mCi $^{128}\text{I/g I}$	2.00E-03		
Properties of Second Batch of ^{128}I -traced Iodine ^a			
q_2/Q_2 , flow-rate ratio	4.15E-08		
Specific activity, mCi $^{128}\text{I/g I}$	9.58E+00		
Elapsed Exposure Time, days	286	350	
Gas-phase Inlet Flow Ratio (q_1/Q_1), g-atoms $^{128}\text{I/g-atom I}$	2.05E-08	9.73E-09	
Gas-phase Inlet Specific Activity, mCi $^{128}\text{I/g I}$	3.52E-01	1.68E-01	
Gas-phase Exit Specific Activity, mCi $^{128}\text{I/g I}$	1.49E-01	9.42E-02	
Sorbed-phase Inventory Ratio (n_1/N_1), g-atoms $^{128}\text{I/g-atoms I}$	8.65E-09	5.47E-09	
Sorbed-phase Specific Activity, mCi $^{128}\text{I/g I}$	1.49E-01	9.42E-02	
Ratio of gas-phase to condensed-phase specific radioactivity [also = $(q_1/Q_1)/(n_1/N_1)$]	2.36	1.78	
Reported DF^*	4. E+4	9. E+3	
Calculated DF (for bulk iodine)	1.69E+4	5.07E+3	

^aThe reference time for the second batch is the zero time of the first batch.

at 196 days, were used to calculate additional values of bulk DFs, namely 1.7×10^4 at 286 days and 5.1×10^3 at 350 days. In essence, the data for exposures of 35, 77, 286, and 350 days show bulk DFs of 4×10^3 to 2×10^4 ; the geometric mean is 8.1×10^3 and the uncertainty is 2.1 to 1/2.1 times the mean. These four values show that, within a factor of 2, the bulk DF for iodine did not change during the 350 days of the test; loading at 350 days was about 9.2 mg of I_2 per milliliter of the 26% (Ag^+ for Na^+ exchanged) silver zeolite. It should be noted that the values for the DF^*/DF ratio at 286 and 350 days are based on 100% exchange of iodine nuclides between gas and condensed phases; such complete exchange ($f = 1$) makes the data at the longer times compatible with those at shorter times. Values of f somewhat less than 1 (perhaps as low as 0.9) might similarly be consistent with the data.

The data of Ackley and Davis¹⁰ on CH_3I trapping are not subject to as nearly unique interpretation as are the iodine data. Instead, the following hypotheses are equally valid:

- (1) There was no exchange between iodine trapped as I_2 and that introduced as CH_3I . In this case, the tracer DFs (DF^*) are equal to the DFs for bulk CH_3I .
- (2) Complete exchange occurred between iodine trapped as I_2 and that introduced as CH_3I . In this case, there is no physically significant solution to Eq. (38).
- (3) There was partial exchange between iodine trapped as I_2 and that introduced as CH_3I . In this case, as in Case 2, DF^* and DF are not equal.

Equation (38) can be greatly simplified when the pertinent experiment involves a very brief injection of one chemical species into a sorbent that already contains sorbate in a different chemical form — CH_3I and I_2 in this case. Since ^{130}I was used to trace CH_3I while ^{128}I was used to trace I_2 , the variables in Eq. (38) have the following values: $n_1^0 (^{130}I) = 0$ in all CH_3I injection tests; the quantity of iodine deposited as CH_3I was very small compared with that

previously deposited as I_2 , in which case $N_1 \approx N_1^0$, or $N_1^0/N_1 \approx 1$. With these boundary conditions,

$$\frac{DF^*}{DF} \approx \frac{1}{1-f}.$$

The ratio of DFs for $CH_3^{130}I$ and $CH_3^{127}I$ cannot be determined since f is not known. A plot of this ratio vs f is similar to the upper curves in Fig. 3. Thus, for example, DF^*/DF has the values 1., 1.91, and 14.6, respectively, when f assumes the values 0.0, 0.5, and 0.98.

Only in Case 1, which may be valid (but is not known to be), do the data on CH_3I trapping have a simple interpretation. The possibility that Case 3 is valid means, in terms of the present model, that the magnitude of the bulk DF for CH_3I on the 26% (Ag^+ for Na^+ exchanged) silver zeolite cannot be specified. To obtain unambiguous values of this DF for CH_3I , it will be necessary to perform long-term tests, such as those performed with iodine, in which reference data are obtained with CH_3I at two successively higher tracer levels. The extent of exchange of iodine between gaseous and sorbed CH_3I could be determined from such measurements.

5. DISCUSSION AND CONCLUSIONS

The model for trapping of short- and long-lived (including stable) isotopes of a chemical element presented in this report is based on simple concepts, namely, material balances across the trap, material recycle, and isotopic exchange. In the case of iodine trapping, the sorbate could be gaseous iodine in an air stream and the sorbent could be a solution of $Hg(NO_3)_2$ in HNO_3 or a bed of silver zeolite. Material-balance equations such as (1) and (2), or (18)-(21), include loss of a short-lived isotope by decay; the role of exchange is contained in Eq. (8) for a no-recycle system and in Eq. (33) for a particular recycle system. Two applications of the model are discussed in the following paragraphs.

In a nuclear fuel reprocessing plant, the specific activity of ^{131}I will be approximately independent of time after initial shakedown operations. The model predicts, for a no-recycle system, that the decontamination factor

for ^{131}I , namely DF^* , will increase uniformly as long as iodine inventory on the sorber is significantly less than the sorber capacity, that is, as long as the decontamination factor for bulk iodine, DF , remains constant and if complete isotopic exchange occurs between iodine in the sorbate and that in the trap. If the exchange is less than complete, the DF^*/DF ratio will increase to an approximately constant value that depends on the extent of exchange. Incipient exhaustion of the trap - namely breakthrough - will correspond to a cessation of increase in DF^*/DF . Depending on the value of DF for the trap, the DF^*/DF ratio could increase to 30 or more during 400 days of operation of a trap for ^{131}I in ^{127}I or ^{129}I ; that is, ^{131}I will be removed in the order of 30 times more effectively, because of its radioactive decay, than will the other two isotopes, as shown in Figs. 2 and 4 for complete isotopic exchange. In a process involving recycle, the decontamination factors of all isotopes will be lower than those of a no-recycle system by amounts that can be accurately calculated from the mass-balance equations if the degree of exchange is known.

In a laboratory experiment, the common use over an extended period of time of a batch of traced iodine corresponds to a specific activity that decreases with time. As long as this same batch of traced iodine is used, the decontamination factors for tracer and bulk iodine remain equal, regardless of the degree of chemical exchange. However, when a second batch is introduced into a trap that has been previously exposed to iodine with a lower or a higher specific activity, the decontamination factors for tracer and bulk iodine will not be equal unless there is no isotopic exchange. Laboratory experiments performed sequentially with iodine at two significantly different specific activities can be used to measure both the efficiency of a trap and the degree of isotopic exchange.

The fractional isotopic exchange, f , is a function of physicochemical processes that have not been described in the derivations in this report. Such processes include physical adsorption and chemical reactions on solids, dissolution, and chemical reaction in solutions. All of these processes are temperature-dependent; the chemical reactions are time-dependent. In addition, mass transfer rate could be an important variable

in the evaluation of f . Whereas the number of experiments from which f can be calculated is small, there are apparently no data from which the kinetics of isotopic exchange, on zeolites, in solution scrubbers, etc., can be analyzed. In the absence of such data, it is not possible to define the range over which several process variables, such as flow rates, bed retention time, sorbate concentration, temperature, etc., may change without producing a significant change in f .

6. ACKNOWLEDGMENTS

The author thanks D. E. Arnurius, R. G. Wymer, and O. O. Yarbrow for helpful discussions during development of the concepts presented in this report.

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8. APPENDICES

6.1 Appendix A: Fuel Reprocessing Plant Calculations

The computer subroutine FRP listed in this Appendix is based on Fig. 1(b) and Eqs. (18)-(34). Calculations are performed up to statement 151; calculated values are stored for printing or plotting between statements 151 and 401. If the number of cases in a set of data is less than 8, the calculated values are printed according to statements between 401 and 451; if the number of cases in a set of data exceeds 8 (but must not exceed 20 with the listed dimensions), the calculated values of DF^*/DF are plotted by use of statements between 451 and 571. The plotting package has previously been described.^{11,12} Figures 4 and 6(a) were plotted in this manner.

Input required at statement 41 + 1 is described in comment cards of subroutine FRP; other input at statements 51 and 51 + 1 is associated with terms defined in Sect. 2 and in the following table:

<u>Program variable</u>	<u>Algebraic variable</u>	<u>Program variable</u>	<u>Algebraic variable</u>
DF	DF	Q(1,1)	Q_1
HAFLEF	t_1/s	QRATIO	q_1/Q_1
END(1,1)	N_1^0	TIMEO	Zero time (usually 0.)
END(1,2)	N_1^0	RECYCL	R
FRAC	f	TEMAX	Time to load sorbent to N_1 (max)


```

150 0020      61 IF (X .GT. 20) GO TO 401
150 0030      T00000 = Q(1,1) * T00000
150 0031      F0010 = J000 - F0000
150 0032      X = X + 1
150 0033      FL = 0.000000000 / 0.000000000
150 0034      HALP = 0.500 * X
150 0035      S = 0
150 0036      Q(1,2) = 0.000000000 * Q(1,1)
150 0037      V(1) = 0.000000000
150 0038      V(2) = 0.000000000
150 0039      V(3) = 0.
150 0040      V(4) = 0.
150 0041      T = T00000
150 0042      DO 101 J = 1, N0001
150 0043      DO 151 I = 1, I0000
150 0044      Q(0,1) = 0.000000000 * V(3)
150 0045      A(1) = Q(1,1) * Q(0,1)
150 0046      Q(0,2) = 0.000000000 * V(4)
150 0047      A(2) = Q(1,2) * Q(0,2)
150 0048      A(3) = FL * V(2)
150 0049      A(4) = FL * V(4)
150 0050      Q0000 = A(1) * J000 - 0.000 / 0.000 - A(1)
150 0051      Q(2,1) = A(1) / 0.000
150 0052      Q(3,1) = (V(1) / F0000) * Q0000
150 0053      IF (V(1) .GT. 0.0) GO TO 111
150 0054      Q(2,2) = (F0010 * A(2) / A(1)) * Q(2,1)
150 0055      Q(3,2) = 0.0
150 0056      GO TO 101
150 0057      111 Q(2,2) = (F0010 * A(2) / A(1)) * F0000 * V(2) / V(1) * Q(2,1)
150 0058      Q(3,2) = (V(2) / V(1)) * Q(3,1)
150 0059      101 F(1) = Q(1,1) - Q(2,1) - Q(3,1) * Q(0,1) - A(1)
150 0060      F(2) = Q(1,2) - Q(2,2) - Q(3,2) * Q(0,2) - A(2)
150 0061      F(3) = Q(1,1) - Q(2,1) - A(3)
150 0062      F(4) = Q(1,2) - Q(2,2) - A(4)
150 0063      CALL 001000
150 0064      IF (T000) 101, 151, 101
150 0065      151 CONTINUE
150 0066      CAPAC(N) = 0.000000000
150 0067      DPSTAB(J,K) = Q(1,1) / Q(2,1)
150 0068      DPSTAB(J,K) = Q(1,2) / Q(2,2)
150 0069      RN(1,1) = V(1)
150 0070      RN(1,2) = V(2)
150 0071      RN(2,1) = V(3)
150 0072      RN(2,2) = V(4)
150 0073      RN011(N) = RN(1,1)
150 0074      RN11(N) = RN(1,1)
150 0075      RN012(N) = RN(1,2)
150 0076      RN12(N) = RN(1,2)
150 0077      Q11(N) = Q(1,1)
150 0078      Q12(N) = Q(1,2)
150 0079      RATIO1(J,K) = DPSTAB(J,K) / 0.000
150 0080      RATIO2(J,K) = DPSTAB(J,K) / 0.000
150 0081      PRSTCL(N) = 0.000000000
150 0082      S00(N) = 0.000000000
150 0083      SPRAC(N) = PRAC
150 0084      SRT_LF(N) = HALP
150 0085      ST(J) = 1
150 0086      301 CONTINUE
150 0087

```

```

150 0000      GO TO 51
150 0001      401 CONTINUE
150 0002      IF (X .GT. 0) GO TO 451
150 0003      WRITE (NO, 1001)
150 0004      WRITE (NO, 1101) (XDF(I), I = 1, N)
150 0005      WRITE (NO, 1111) (XDF01(I), I = 1, N)
150 0006      WRITE (NO, 1121) (XDF02(I), I = 1, N)
150 0007      WRITE (NO, 1131) (XDF1(I), I = 1, N)
150 0008      WRITE (NO, 1141) (XDF2(I), I = 1, N)
150 0009      WRITE (NO, 1151) (XDFAC(I), I = 1, N)
150 0010      WRITE (NO, 1161) (XDFLIF(I), I = 1, N)
150 0100      WRITE (NO, 1171) (XDFAC(I), I = 1, N)
150 0101      WRITE (NO, 1181) (XDFAC(I), I = 1, N)
150 0102      WRITE (NO, 1201)
150 0103      DO 421 J = 2, NNNL, 2
150 0104      WRITE (NO, 1211) ST(J), (RATIO2(J,L), L = 1, N)
150 0105      421 CONTINUE
150 0106      WRITE (NO, 1001)
150 0107      WRITE (NO, 1221)
150 0108      DO 431 J = 2, NNNL, 2
150 0109      WRITE (NO, 1211) ST(J), (RATIO1(J,L), L = 1, N)
150 0110      431 CONTINUE
150 0111      GO TO 41
150 0112      451 READ (UI, 911) HEIGHT, WIDTH, ANG1, ANG2, RUI12, TICAL, SHADGW
150 0113      READ (UI, 921) W1, DEL1, W2, DEL2, W1V1, DEL1, LTWO
150 0114      READ (UI, 931) (IDGT(J), J = 1, 12)
150 0115      READ (UI, 931) (JDDAW(J), J = 1, 12)
150 0116      READ (UI, 931) WOB, (LOG(L), L = 1, NNN)
150 0117      DO 571 LL = 1, NNN
150 0118      L = LOG(LL)
150 0119      CALL BOX (HEIGHT, WIDTH, ANG1, LOG2, RUI12, SHADGW, W1, DEL1,
150 0120      W2, DEL2, W1V1, DEL1, IDGT, LTWO, AA)
150 0121      CALL MARK (JDDAW, W1, TICAL, W2, DEL2, W1V1, DEL1, TICAL)
150 0122      DO 521 I = 1, N
150 0123      X2 = SPFRAC(I)
150 0124      CALL CURVE(0.0, X2, 1.0, L, 1)
150 0125      DO 511 J = 1, NNNL
150 0126      X1 = ST(J)
150 0127      YP1 = RATIO2(J, I)
150 0128      CALL CURVE(X1, X2, YP1, L, J + 1)
150 0129      511 CONTINUE
150 0130      CALL CURVE(X1, X2, 1.0, L, J)
150 0131      521 CONTINUE
150 0132      CALL CURVE(0.0, 0.0, 1.0, L, 1)
150 0133      CALL CURVE(ST(NNNL), 0.0, 1.0, L, 2)
150 0134      CALL CURVE(0.0, 1.0, 1.0, L, 1)
150 0135      CALL CURVE(0.0, 0.0, 1.0, L, 2)
150 0136      DO 551 I = 10, NNNL, 10
150 0137      X1 = ST(I)
150 0138      DO 541 J = 1, N
150 0139      X2 = SPFRAC(J)
150 0140      YP1 = RATIO2(I, J)
150 0141      CALL CURVE(X1, X2, YP1, L, J)
150 0142      541 CONTINUE
150 0143      CALL CURVE(X1, 0.0, 1.0, L, N)
150 0144      551 CONTINUE
150 0145      CALL ADVANC(I)
150 0146      571 CONTINUE

```

```

ISB 0146      43  T3  01
ISB 0147      401  WRITE (NO, 1001)
ISB 0148      401  FORMAT (2I5, 10.0)
ISB 0149      411  FORMAT (0E10.0)
ISB 0150      421  FORMAT (3(I5, 10.0), 15)
ISB 0151      431  FORMAT (12I2)
ISB 0152      1001  FORMAT (10I1)
ISB 0153      1101  FORMAT (' STABLE-ISOTOPE OF', 1P0E10.1)
ISB 0154      1111  FORMAT (' INITIAL STABLE-ISOTOPE INVENTORY, 1-GMOLES', 1P0E10.3)
ISB 0155      1121  FORMAT (' INITIAL RADIOACTIVE-ISD. INVENTORY, G-GMOLES', 1P0E10.1)
ISB 0156      1131  FORMAT (' ELEMENT TOTAL FLOW RATE, G-GMOLES/DAY', 1P0E10.1)
ISB 0157      1141  FORMAT (' RADIOACTIVE ISOTOPE FLOW RATE, G-GMOLES/DAY', 1P0E10.3)
ISB 0158      1151  FORMAT (' FRACTIONAL ISOTOPE EXCHANGE', 1P0E10.1)
ISB 0159      1161  FORMAT (' HALF LIFE OF ISOTOPE, DAYS', 1P0E10.3)
ISB 0160      1171  FORMAT (' RES CAPACITY FOR IONIC GRAB-ATONS', 1P0E10.1)
ISB 0161      1181  FORMAT (' THE FRACTIONAL PRECISE IN THIS CASE IS', 1P0E10.3)
ISB 0162      1201  FORMAT ('//', TIME, - - - -
1- - - - OF (SHORTEST HALF-LIFE ISOTOPE) / OF (EQUIPMENT) - - - -
2- - - - / DAYS
1
0
0 /)
ISB 0163      1211  FORMAT ('', 1P0E10.1)
ISB 0164      1221  FORMAT ('//', TIME, - - - -
1- - - - OF (LONG HALF-LIFE OR STABLE ISOTOPE) / OF (EQUIPMENT) - - - -
2- - - - / DAYS
1
0
0 /)
ISB 0165      RETURN
ISB 0166      END

```

2. Appendix B: Calculation Based on Laboratory Data

The computer subroutine LABW listed on the next three pages was written to solve Eqs. 10 and 30; calls for input between statements -1 and 51 were chosen to utilize the data of Ackley and Davis.¹⁰ Figure 1a is a model of the flow pattern; algebraic and program variables are related in the following table:

<u>Program variable</u>	<u>Algebraic variable</u>	<u>Program variable</u>	<u>Algebraic variable</u>
TIME	Elapsed time when a sample was taken for counting, t	DFSEXP	EF* (experimental)
FLORAT	Gas flow rate for a single sorbent unit	HAS LIF	t/s
CONC	Conc. of I_2 in the inlet air	ENO1	N_1^0
QSATIC	Q_1, Q_2	ENO2	n_1^0
WATWT	Atomic weight of tracer	FRAC	f
WATWTS	Atomic weight of bulk iodine	TIME0	Time at start of exposure. In a run of successive samples, TIME0 is set to -1 after the first sample; this causes the program to set TIME0 to the previous sample time.

LEVEL 21.6 (DEC 72)

CS/360 POSTMAN 8

COMPILER OPTIONS - NAME= NAME, CPT=02, LIBUCLT=60, SIZE=0006K,
SOURCE, EXECIC, DOLIST, DODUCK, LOAD, MAP, DODNET, DRED, DNETP

```

ISW 0002      SUBROUTINE LADDER
ISW 0003      IMPLICIT REAL*8(A-H,O-Z)
ISW 0004      DIMENSION ACTRES(25,10), ACTGSO(25,10), ACTSBO(25,10)
ISW 0005      DIMENSION DFCAL(25,10), DATIO(25,10)
ISW 0006      DIMENSION SDF(25,10), SDO1(25,10), SDO2(25,10)
ISW 0007      DIMENSION SW1(25,10), SW2(25,10), SPAC(25,10), SUPLI(10)
ISW 0008      DIMENSION SQ11(25,10), SQ12(25,10), SQ12(25,10), ST(25)
ISW 0009      COMMON/TAPES/IE, NO, DP, DTTC
ISW 0010      WRITE (NO,1001)
ISW 0011      CON1 = 6.021 * 23 * DLOG(2.000) / 3.7 * 10 / 86400.
ISW 0012      CONVC = 1.00-0
ISW 0013      ONE = 1.000
ISW 0014      ICKOUT = 0
ISW 0015      J = 0
ISW 0016      01 J = J + 1
ISW 0017      READ (NI,901) TIME, FLORET, CONC, QRTIO
ISW 0018      READ (NI,901) CATOT, CATUTS
ISW 0019      K = 0
ISW 0020      51 READ (NI,901) DFXEP, HAPLI, ENO1, ENO2, FRAC, TIMEO
ISW 0021      DP = DFXEP
ISW 0022      IF (DP - ONE) 601, 001, 61
ISW 0023      61 IF (K .GT. 6) GO TO 001
ISW 0024      K = K + 1
ISW 0025      EL = DLOG(2.000) / HAPLI
ISW 0026      Q11 = FLORET * CONC * 1000.00
ISW 0027      Q012 = QRTIO * Q11
ISW 0028      Q11 = Q11 / CATOT
ISW 0029      Q012 = Q012 / CATUTS
ISW 0030      IF (TIMEO .LT. 0.) Q012 = Q012 * DEXP(-EL*ST(J-1))
ISW 0031      IF (TIMEO .LT. 0.) TIMEO = ST(J-1)
ISW 0032      IF (ENO1 .LT. 0.) ENO1 = SW1(J-1,K)
ISW 0033      IF (ENO2 .LT. 0.) ENO2 = SW2(J-1,K)
ISW 0034      DTIME = TIME - TIMEO
ISW 0035      Q21 = Q11 / DP
ISW 0036      DIP = Q11 - Q21
ISW 0037      EN1 = ENO1 * DIP * DTIME
ISW 0038      ICK = 0
ISW 0039      01 ICK = ICK + 1
ISW 0040      IF (ICK .GT. 10) GO TO 121
ISW 0041      EXP1 = FRAC / (DP - ONE)
ISW 0042      TERM1 = (ENO1 / EN1) * EXP1
ISW 0043      TERM2 = ENO2 * Q11 - Q012 * ENO1
ISW 0044      TERM3 = TERM2 / Q11
ISW 0045      EXPT = DEXP(-EL * DTIME)
ISW 0046      EN2 = (TERM1 * TERM3 * Q012 * EN1 / Q11) * EXPT
ISW 0047      TERM = FRAC * TERM2 * TERM1 / EN1
ISW 0048      DFCAL(J,K) = DP * Q012 / (Q012 * TERM)
ISW 0049      T1 = DFXEP / DFCAL(J,K)
ISW 0050      T2 = T1 - CON1
ISW 0051      DP = DP * T1
ISW 0052      IF (DABS(T2) - CONVC) 131, 131, 01
ISW 0053      121 WRITE (NO,1301) J, K, T1, DFXEP
ISW 0054      131 Q21 = Q11 / DP
ISW 0055      DIP = Q11 - Q21
ISW 0056      EN1 = ENO1 * DIP * DTIME
ISW 0057      151 CONTINUE

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ISB 0064      Q12 = Q012 * EXP1
ISB 0065      Q22 = Q12 / SPICAL(J,N)
ISB 0066      251 RATIO(J,N) = DPICAL(J,N) / DP
ISB 0067      ST(J) = TIME
ISB 0068      301 CONTINUE
ISB 0069      SE01(J,N) = SE01
ISB 0070      SE01(J,N) = SE01
ISB 0071      SE01(J,N) = SE01
ISB 0072      SPAC(J,N) = PACC
ISB 0073      SHFLIP(I) = SHFLIP
ISB 0074      SE02(J,N) = SE02
ISB 0075      SE02(J,N) = SE02
ISB 0076      ACT000 = SE02 * C001 / SHFLIP
ISB 0077      ACT000(J,N) = ACT000 / (SE01 * C001)
ISB 0078      ACT001(J,N) = Q12 * C001 / SHFLIP
ISB 0079      ACT001(J,N) = ACT001(J,N) / (SE01 * C001)
ISB 0080      ACT000(J,N) = Q22 * C001 / SHFLIP
ISB 0081      ACT000(J,N) = ACT000(J,N) / (SE01 * C001)
ISB 0082      SQ11(J,N) = Q11
ISB 0083      SQ12(J,N) = Q12
ISB 0084      SQ012(J,N) = Q012
ISB 0085      GO TO 51
ISB 0086      401 CONTINUE
ISB 0087      ICOUNT = ICOUNT + 1
ISB 0088      IF (ICOUNT .LE. 3) GO TO 611
ISB 0089      ICOUNT = 1
ISB 0091      411 CONTINUE
ISB 0092      WRITE (NO,1101) (SE01(J,I), I = 1,N)
ISB 0093      WRITE (NO,1111) (SE02(J,I), I = 1,N)
ISB 0094      WRITE (NO,1121) (SE01(J,I), I = 1,N)
ISB 0095      WRITE (NO,1131) (SE02(J,I), I = 1,N)
ISB 0096      WRITE (NO,1141) (SE02(J,I), I = 1,N)
ISB 0097      WRITE (NO,1151) (SQ12(J,I), I = 1,N)
ISB 0098      WRITE (NO,1151) (SQ11(J,I), I = 1,N)
ISB 0099      WRITE (NO,1171) (SPAC(J,I), I = 1,N)
ISB 0100      WRITE (NO,1181) (SHFLIP(I), I = 1,N)
ISB 0101      WRITE (NO,1201) ST(J), (DPICAL(J,I), I = 1,N)
ISB 0102      WRITE (NO,1211) RATIO(J,N), I = 1,N)
ISB 0103      WRITE (NO,1221) (ACT000(J,I), I = 1,N)
ISB 0104      WRITE (NO,1231) (ACT001(J,I), I = 1,N)
ISB 0105      WRITE (NO,1241) (ACT000(J,I), I = 1,N)
ISB 0106      WRITE (NO,1291)
ISB 0107      501 CONTINUE
ISB 0108      IF (ICOUNT .EQ. 3) WRITE (NO,1001)
ISB 0109      GO TO 41
ISB 0110      601 WRITE (NO,1001)
ISB 0111      901 FORMAT (DE10.0)
ISB 0112      1001 FORMAT ('01')
ISB 0113      1101 FORMAT (' STABLE-ISOTOPE OF',
ISB 0114      1 10X, 1P6E10.3)
ISB 0115      1111 FORMAT (' INITIAL ELEMENT INVENTORY, G-HOLES ',
ISB 0116      1 10X, 1P6E10.3)
ISB 0117      1121 FORMAT (' FINAL ELEMENT INVENTORY, G-HOLES ',
ISB 0118      1 10X, 1P6E10.3)
ISB 0119      1131 FORMAT (' INITIAL RADIOACTIVE-ISO. INVENTORY, G-HOLES ',
ISB 0120      1 10X, 1P6E10.3)
ISB 0121      1141 FORMAT (' FINAL RADIOACTIVE-ISO. INVENTORY, G-HOLES ',
ISB 0122      1 10X, 1P6E10.3)

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ISN 0119      1151 FORMAT (' ELEMENT TOTAL FLOW RATE,          G-HOLES/DAY ',
      1 10X, 1P6E10.3)
ISN 0120      1161 FORMAT (' RADIOACTIVE ISOTOPE FLOW RATE,    G-HOLES/DAY ',
      1 10X, 1P6E10.3)
ISN 0121      1171 FORMAT (' FRACTIONAL ISOTOPIC ENRICHMENT,
      1 10X, 1P6E10.3)
ISN 0122      1181 FORMAT (' HALF LIFE OF ISOTOPE              DAYS ',
      1 10X, 1P6E10.3)
ISN 0123      1201 FORMAT (' SAMPLING TIME AND CALC. DP%,    DAYS AND DP% ',
      1 1P7E10.3)
ISN 0124      1211 FORMAT (' DISCONTINUATION FACTOR RATIO,    DP%/DP% ',
      1 10X, 1P6E10.3)
ISN 0125      1221 FORMAT (' SPEC. ACTIV. OF SORBATE ON SOLVENT,  CI/G ',
      1 10X, 1P6E10.3)
ISN 0126      1231 FORMAT (' SPEC. ACTIV. OF SORBATE, INLET STREAM, CI/G ',
      1 10X, 1P6E10.3)
ISN 0127      1241 FORMAT (' SPEC. ACTIV. OF SORBATE, OUTLET STREAM, CI/G ',
      1 10X, 1P6E10.3)
ISN 0128      1291 FORMAT (//)
ISN 0129      1301 FORMAT (' CONVERGENCE OF CALCULATED DP% TO EXPERIMENTAL VALUE WAS
      1 NOT ACHIEVED IN 10 ITERATIONS. ' /
      2 ' THE LAST VALUE OF (DPSEED/DPSCAL(' , I2, I2, ') WAS ',
      3 ' :P10.3, ' FOR DPSEED = ' , I10.3)

ISN 0130      RETURN
ISN 0131      END

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